

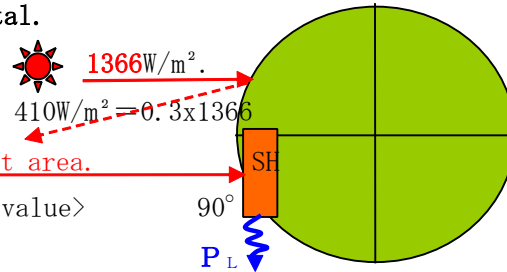
Solar Heater (SH) is the very best performance in energy technology. Below are the physics basis and some design example. You could invent better SH.

<http://solarcooking.org/>

Author is not actual expert on SH, but had been "B wave generator" in energy technology. Also you could see SH is the kernel technology against the Climate Change Crisis. Above all, those are the best cost and CO2 performance than any other else. If you could save foods and energy, you could conquer any threatenning.

[1] : Solar Heater the physics fundamental.

- ①(1) Solar constant = 1366 W/m^2 .
- (2) reflection rate (albedo) $\equiv a \doteq 0.3$.
- (3) direct effective heat input ($\equiv P_s$)/unit area.
 $= 1366 \text{ W/m}^2 \times (1 - 0.3) = 956 \text{ W/m}^2 \dots$ <best value>

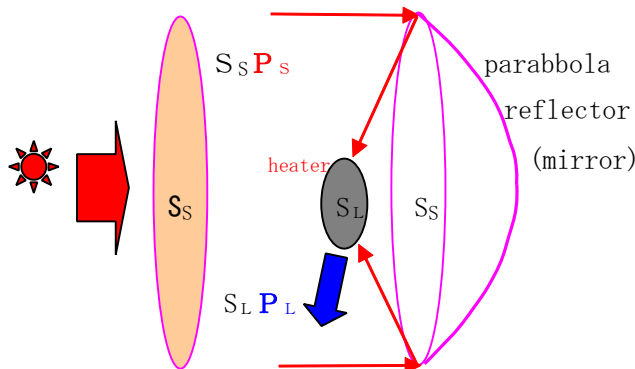


(4) SH light reciever surface is setted perpendicular to incoming beam, so heat amount depend fundamentally not seasonal !!, however seasonal penetrating length of solar ray in atomosphere would attenuate P_s by vapor density, etc.

② solar heat input and dissipated heat output from heater of temperature T.

(1) actual heat input in SH $\equiv P_H = S_s P_s (956 \text{ W/m}^2) - S_L P_L$.
 Effective heat input $\equiv Q_s = S_s P_s$ is uniquely determined by S_s . Heat loss $Q_L = S_L P_L$ depend on thermodynamic design of SH and its thermal enviroment.

(2) $S_s P_s$ is proportional to perpendicular recieving area S_s of incoming solar beam. Similary $S_L P_L$ is too. S_L is total surface area of heat container of T. Dissipated radiataion thermal loss $\equiv P_L$ /unit area might depend material of heater and the enviromental temperature, wind, etc.



Note that incoming sun beam are almost visible ray and some infrared one (IR). While dissipated heat output are infrared ray to space, and conductive and covection heat flow in air and insulator.

Hence larger S_s and smaller S_L are preferable for getting larger effective heat.

(3) **Heat Loss Estimation = dissipated thermal loss by radiation** $\equiv Q_L = S_L \sigma T^4$.

In SH design, P_L is called Blackbody Radiation ($= \sigma T^4$) and is serious important.

Example-1)

$$\sigma T^4 = 5.67 \times 10^{-8} \times (273 + 40^\circ\text{C})^4 = 544 \text{W/m}^2. \quad \langle\langle \text{bath water temperature} \rangle\rangle$$

$$\sigma T^4 = 5.67 \times 10^{-8} \times (273 + 100^\circ\text{C})^4 = 1100 \text{W/m}^2. \quad \langle\langle \text{boiling water temperature} \rangle\rangle$$

Boiling pan & kettle of "unit area" has larger heat loss as shown in above.

(4) **Countermeasure for heat loss:**

(a) making **smaller heating surface area S_L** . \rightarrow spherical surface is the best.

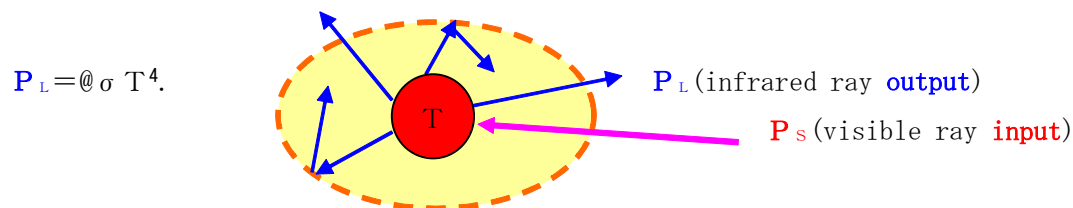
Example-2)

2.2 liter kettle has 0.12m^2 surface area $= S_L \rightarrow$

$$S_L \sigma T^4 = 0.12 \times 5.67 \times 10^{-8} \times (273 + 100^\circ\text{C})^4 = 132 \text{W/m}^2. \quad (@=1 \text{ of blackbody}).$$

$$@S_L \sigma T^4 = 0.5 \times 0.12 \times 5.67 \times 10^{-8} \times (273 + 100^\circ\text{C})^4 = 62 \text{W/m}^2. \quad (@=0.5 \text{ of graybody}).$$

(b) **green house method** of $@$ (heat (infrared ray) reflecting wall $\equiv \text{HW}$).



HW allow passing of visible ray P_s , while, HW can reduce **passing probability** $@$ of infrared ray (IR) from heating kernel T , which can rise temperature T .

(c) **maximum temperature rise realizing by $@$ of HW.** $0 < @ < 1$.

In heat flow balanced state, $S_S P_s = S_L P_L$.

$$S_S P_s = S_L @ \sigma T^4. \rightarrow P'_s \equiv (S_S/S_L) P_s / @ = \sigma T^4 \geq (S_S/S_L) P_s.$$

$$\rightarrow T_{\text{Max}} = [(S_S/S_L) P_s / @ \sigma]^{1/4}.$$

Example-3) $\ast \sigma = 5.67 \times 10^{-8} \text{W/m}^2 \text{K}^4$. (Stefan Boltzman constant).

$$@=1.0, \rightarrow P_s (956 \text{W/m}^2) = @ \sigma T^4. \rightarrow T = (P_s / \sigma)^{1/4} = 360 \text{K} = (273 + 87^\circ\text{C}).$$

$$@=0.5, \rightarrow P_s (956 \text{W/m}^2) = @ \sigma T^4. \rightarrow T = (P_s / @ \sigma)^{1/4} = 429 \text{K} = (273 + 156^\circ\text{C}).$$

$\Rightarrow T = 150^\circ\text{C}$ is told sufficient for slow mode cooking.

http://solarcooking.wikia.com/wiki/Minimum_Solar_Box_Cooker

<http://solarcooking.org/>

(5) realizing green house by insulators {**glass, vinyl, ..., paper board**}.

Those materials have $@ < 1$ against infrared ray.

(6) heat insulator materials.

air, glass wool, paper board, aluminium foil, ...

(7) heat absorber by black paint.

Heat container surface must be black color for enhancing heat input.

③ On the global green house effect and $P_G \equiv 1566 \text{W/m}^2$.

(1) The emergent crisis of the global warming (Climate Change Crisis \equiv CCC) is caused by **Heat Trapping Gas** (Green House effect Gas \equiv GHG*) in atmosphere.

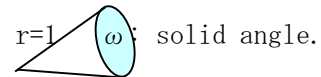
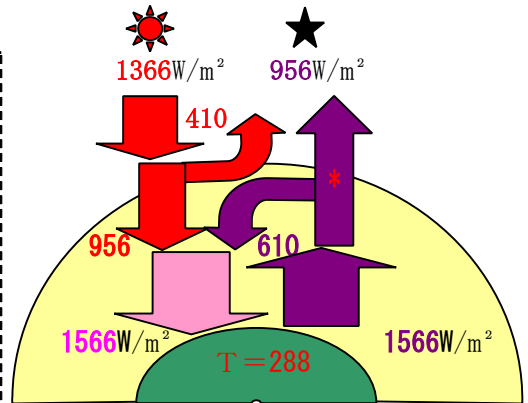
See below figure.

$$P_s (956 \text{W/m}^2) = @ \sigma T^4 \dots \dots \dots [1] \textcircled{2} (4)(b)$$

$$@ = (956 \text{W/m}^2) / (1566 \text{W/m}^2) = 0.61. \ll \text{passing probability of IR from earth} \gg.$$

$$\sigma T^4 = 5.67 \times 10^{-8} \times (273 + 15^\circ\text{C})^4 = 1566 \text{W/m}^2. \ll \text{Black body radiation from } T = 288 \gg.$$

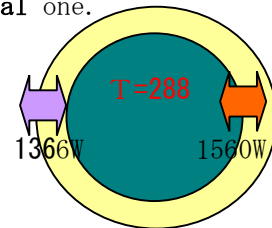
(2) Heat input on globe is not only direct solar ray (DS = 956W/m^2), but also infrared ray reradiation from GHG = heat trapping gas (RG = 610W/m^2) in atmosphere. Then DS is one directional beam, while RG is isotropical one (visible sky solid angle = ω from SH receiver surface). If ω could be 2π , heat input = 610W/m^2 , if $\omega = \pi/8$, input = 40W/m^2 ?



(3) Conclusion on 610W/m^2 heat input:

$$1566 \text{W/m}^2 = 956 \text{W/m}^2 + 610 \text{W/m}^2.$$

610W/m^2 is a big heat amount, but substantially not available for SH. Because SH is an antenna of uni-directional, while RG needs all-directional one.



(4) Heat account at earth surface and stratsphere boundary.

(a) earth surface: $1566 \text{W/m}^2 = 956 \text{W/m}^2 + 610 \text{W/m}^2$.

(b) stratsphere boundary: $1366 \text{W/m}^2 = 956 \text{W/m}^2 + 410 \text{W/m}^2$.

(c) The real cause of CCC is caused from Heat Passing Rate \equiv @ decreasing by GHG.

$$\pi R_E^2 P_s (1-a) = 4 \pi R_E^2 @ \sigma T_E^4. \rightarrow T_E = [P_s (1-a) / 4@ \sigma]^{1/4}.$$

If @ decreased, T becomes higher. $\ll R_E = \text{earth radius}, T_E = \text{global temperature} \gg$

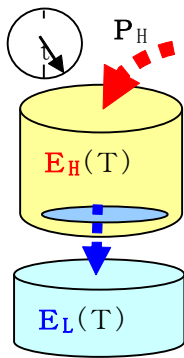
(d) The real cause of global warming is caused from Heat Debt.

surplus heat (radiative forcing \equiv RF = 1.6W/m^2) = heat input - heat output.

By decreasing @, cooling radiation from earth is more trapped to increase 1560W.

Strictly to tell on heat balance (4)(a)(b), those have deficit RF = 1.6W/m^2 , which has been reseeded in ocean heat (99.9% heat capacity of earth!!) and cause global warming (turbulence energy of ocean and atmosphere causing climate disasters, such as big floods, big draught, extreme weather, strong hurricane, ...).

[2] : How much **heat amount** $\equiv E_H$ and **boiling time** $\equiv t_H$ "does SH take ??".



$$E_H = C_H(T_M - T_0) = \text{Heat capacity} \times \text{Temperature rise} = \text{necessary energy}$$

$$P_H = Q_S - Q_L = S_S P_S - S_L P_L = E_H / \langle t_H \rangle. \langle \text{heat input/unit time} \rangle$$

$$E_S - E_L = E_H = P_H \langle t_H \rangle = \int_0^{t_H} dt P_H(t). \langle \text{heating up time} \rangle$$

$$E_H + E_L = E_S = Q_S \langle t_H \rangle. \langle t_H = \text{time for getting max temperature} = T_M \rangle$$

$$Q_S = S_S P_S. \langle \text{solar heat input per unit time} \rangle.$$

$$Q_L = S_L \sigma T^4. \langle \text{heat loss per unit time at temperature } T \rangle.$$

(Total heat for boiling E_H + Total heat loss E_L) / heat input (watt) Q_S
= heating time t_H .

① **bath** (the maximum heat consumer in home living!!!).

Take caution on loss heat by cooling radiation accompanied with T rise.

(1) unit T rise heat/unit weight = **water specific heat** = $4.178 \text{KJ}/^\circ\text{CKg}$.

(2) bath water weight = $0.8\text{m} \times 0.6\text{m} \times 0.3\text{m} \times 1000\text{kg}/\text{m}^3 = 150\text{kg}$.

(3) Q_B = heat capacity/ 1°C = $4.178\text{KJ}/\text{Kg}^\circ\text{C} \times 150\text{kg} = 630\text{KJ}/^\circ\text{C}$.

(4) Total heat = $Q_B \times (40 - 10^\circ\text{C}) = 30^\circ\text{C} \times 630\text{KJ}/^\circ\text{C} = 18900\text{KJ}$. ?!

$\ll \text{☞} : 24 \text{ times of } 781\text{K} = 2.21 \text{ boiling kettle heat amount!!!} \gg$.

(5) dissipated radiation heat loss in heat input = $364(10^\circ\text{C})$, $544(40^\circ\text{C}) \text{W}/\text{m}^2$.

(6) warm up time $\doteq 18900\text{KJ} / \langle (956\text{W}/\text{m}^2 \times 1.5\text{m}^2 - 544\text{W}/\text{m}^2) \times 3600 \rangle = 5.9\text{h}$

$\text{☞} : \text{Solar ray receiving area } S_S = 1.5\text{m}^2$. equivalent dissipated area = 1m^2 .

Commercial product has almost 2m^2 , water temperature gradient automatically circulate wamer water to heat reserver tank, which finally supply bath water.

② **kettle** (2.2liter = 2.2Kg, heat capacity $\equiv C = (4.178\text{KJ}/\text{Kg}^\circ\text{C} \times 2.2\text{Kg})$)

(1) Q_K necessary heat = $C \times (100 - 15)^\circ\text{C} = (4.178\text{KJ}/\text{Kg}^\circ\text{C} \times 2.2\text{Kg}) \times (100 - 15)^\circ\text{C} = 781\text{KJ}$.

(2) heat loss : $L = \sigma T^4 = 5.67 \times 10^{-8} \times (283)^4 = 364\text{W}/\text{m}^2$.

$$L = \sigma T^4 = 5.67 \times 10^{-8} \times (373)^4 = 1100\text{W}/\text{m}^2.$$

$\text{☞} : \text{In air, heat loss by condution and covection is so small and neglegible.}$

(3) **cooling radiation area** $S_L = 4\pi R^2 = 4\pi (0.15\text{m})^2 = 0.3\text{m}^2$. $\rightarrow \langle L \rangle \doteq 300\text{W}/\text{m}^2$.

(4) $Q_K = 781\text{KJ} / 0.5\text{h}(\text{boiling time}) \times 3600\text{s}/\text{h} \doteq 400\text{W}$, + 300W . $700\text{W} \rightarrow S_S \doteq 1\text{m}^2$.

$\text{☞} : \text{Heat loss is almost same as net heat, so loss must be decreased. Boling time is a criterion of SH performance. Note heat loss increases as } T \text{ gose higher.}$

(5) Strict solution of temperature rise process:

$$: P_H = Q_S - @ S_L \sigma T^4 = C dT/dt.$$

$$= 700\text{W} - 100\text{W}(283) \doteq C \langle dT/dt \rangle. \quad \langle \langle T = 0.36\text{h} \rangle \rangle$$

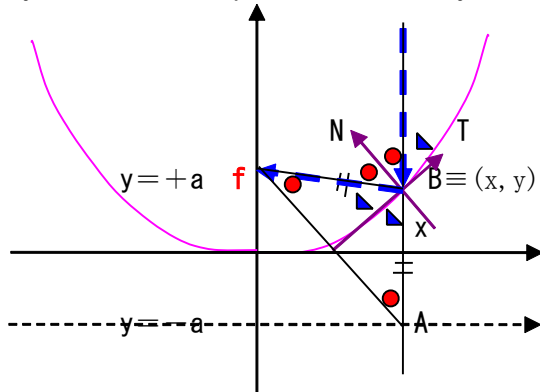
$$= 700\text{W} - 300\text{W}(373) \doteq C \langle dT/dt \rangle. \quad \langle \langle T = 0.54\text{h} \rangle \rangle$$

[2] : Principle of parabola solar ray collector.

Commercial SH bath wamer has not ray collector, but those has wider ray reciver area of water circulating pipe line within heat insulator box and with heat reserver tank. Pipe line and insulator box become high cost. Below technique are simple for mono heater tank (smaller S_L with rather high temperature), but accurate parabola antenna (wider S_S) is rather difficult for amateure fabrication.

(1) Parabola surface and focus coordinate f .

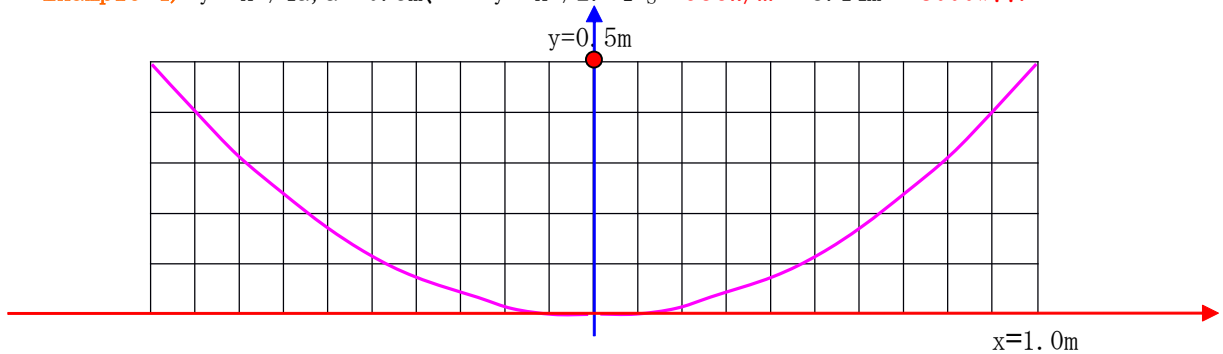
$$AB = y + a \equiv \sqrt{(x^2 + (a-y)^2)} = Bf. \quad \rightarrow \quad y = x^2/4a.$$



T and N are tangential and normal line at $B \equiv (x, y = x^2/4a)$. Then all incoming light beam being pararell with y axis is to be focused at $f(0, a)$. Thus **higher temperature** can be gotten.

(2) Parabolar of commercial goods has opening radius = 0.8 ($P_S = 1900W$) \sim 1.5m ($P_S = 6700W$), and focus point is about 0.5m from bottom,

Example-4) $y = x^2/4a, a = 0.5m, \rightarrow y = x^2/2, P_S = 956W/m^2 \times 3.14m^2 = 3000W!!$.



x=0	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9	1.0
y=0	.005	0.02	.045	0.08	.125	0.18	.245	0.32	.405	0.5

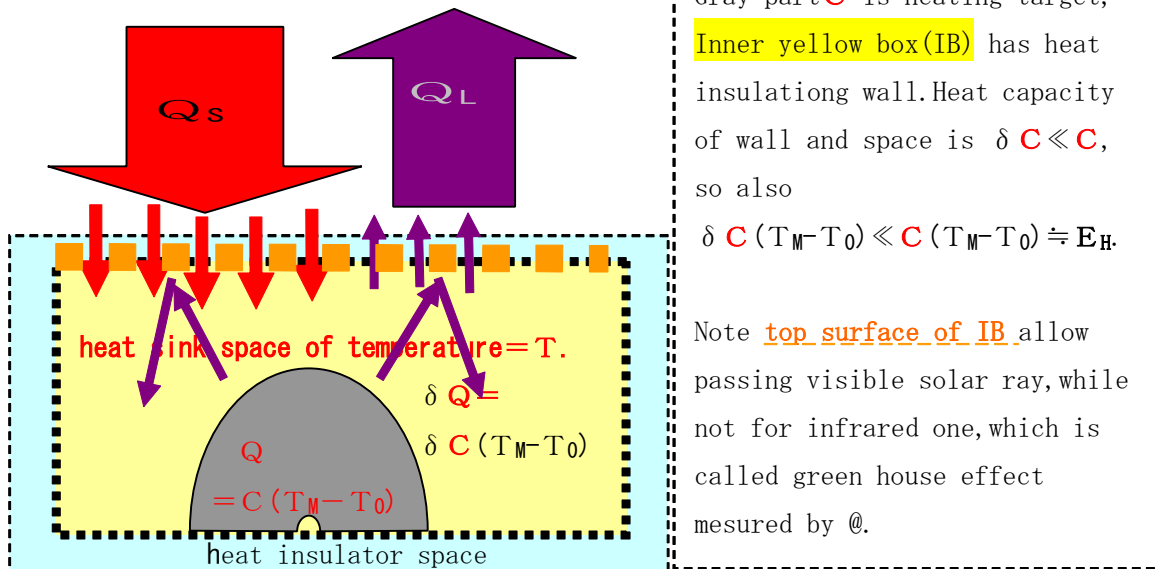
Parabola $r = 0.50m, \rightarrow S = \pi r^2 = 0.78m^2 \rightarrow P = 956W/m^2 \times 0.78m^2 = 745W$.
$r = 0.75m, \rightarrow S = \pi r^2 = 1.77m^2 \rightarrow P = 956W/m^2 \times 1.77m^2 = 1689W$.

Boiling time is 30 minutes for 2.2liter kettle of $\langle 10^\circ C \rightarrow 100^\circ C (781KJ) \rangle$.

$$T = 781KJ / (745W - 300W) \times 3600 = 0.5h.$$

[3] : Green House Effect Box without solar ray focusing.

In a temperature equilibrium space, heat tend to be collected in larger heat capacity portion. This could be replaceable with heat beam focusing method for getting higher temperature T.



In a thermal equilibrium state, incoming and outgoing heat are balanced.

Conductive and convection heat flow loss are almost negligible.

$$(1) Q_s = P_s S_s = 956 \text{ W/m}^2 \times S_s.$$

$$(2) Q_s = Q_L = S_L \sigma T^4. \rightarrow (3) T_M = [Q_s / S_L \sigma]^{1/4}. \langle \text{equilibrium max temperature} \rangle$$

$$(4) E_H = C_H (T_M - T_0).$$

$$\{(5) Q_L(T_0) = S_L \sigma T_0^4; \quad (6) Q_L(T_M) = S_L \sigma T_M^4\}.$$

$$(7) t_H \doteq E_H / (Q_s - \langle Q_L(T_0) + Q_L(T_M) \rangle / 2). \langle \langle \text{coarse estimation} \rangle \rangle$$

To gain higher temperature in (3), $S_L \sigma$ should be smaller in SH design.

To gain short taking time t_H , Q_s should be larger.

Example-5)

inner blackbody box size = $0.46 \text{ m} \times 0.36 \text{ m} \times 0.18 \text{ m}$; opening area $S_s = 0.46 \times 0.36 = 0.16 \text{ m}^2$.

input heat amount $Q_s = 900 \text{ W/m}^2 \times 0.16 \text{ m}^2 = 150 \text{ W}$. $\rightarrow 80^\circ \text{C}$ <observing 2011/2/3 in Japan>.

cooling radiation area $S_L = 2(0.46 \times 0.36) + 2(0.46 \times 0.18) + 2(0.18 \times 0.36) = 0.312 \text{ m}^2$.

(1) convection heat flow into exterior air $Q_{LC} = S_L J = 0.312 \text{ m}^2 \times 7 \text{ W/m}^2 \text{K}$. <negligible>

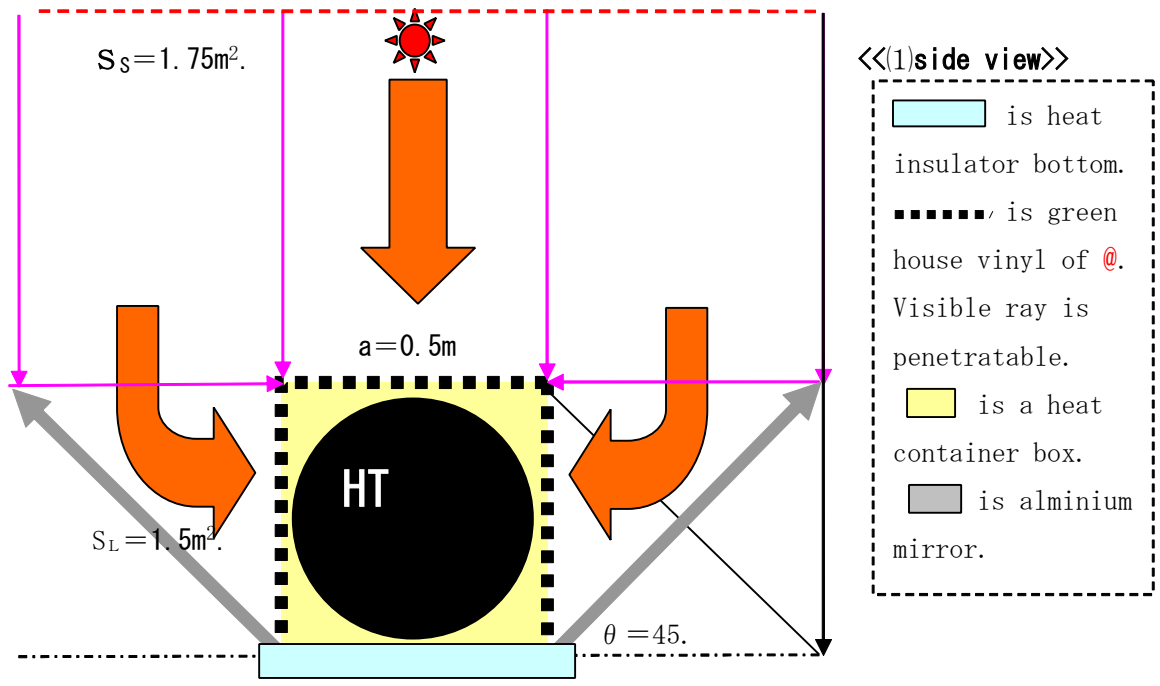
(2) radiation rate of material surface $\epsilon \doteq 0.5$?

Max cooling radiation amount $Q_s = Q_L = S_L \epsilon \sigma T^4. \rightarrow T \doteq 87^\circ \text{C}$, observing = 80°C ,

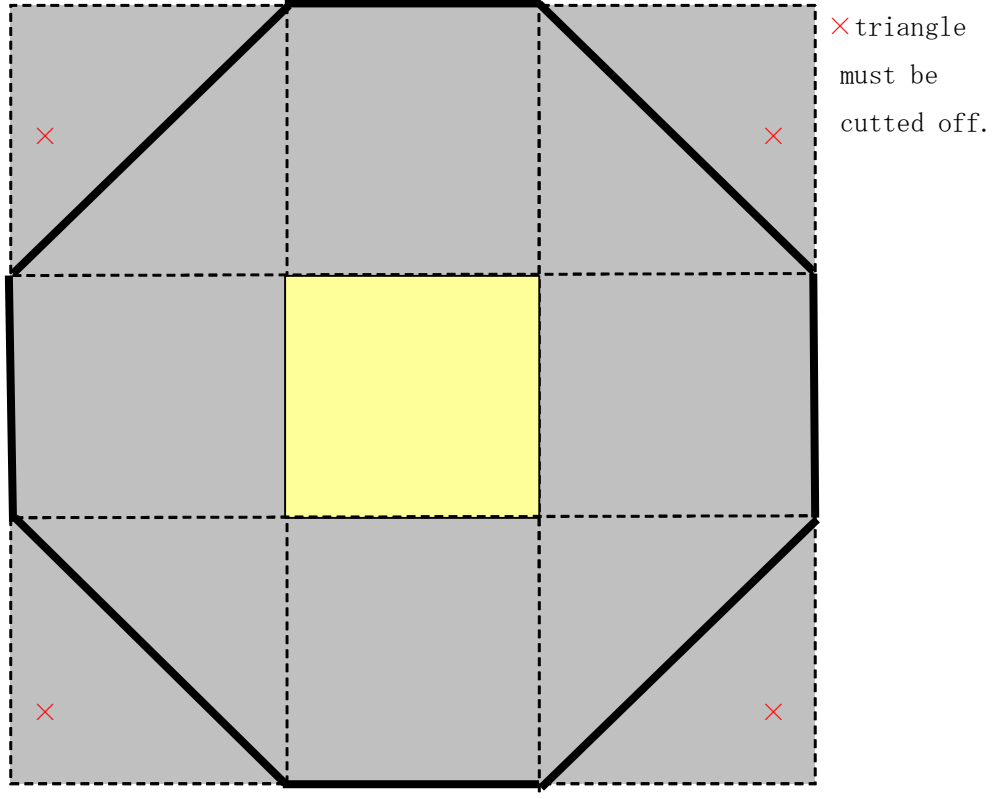
*reference site on heat calculation.

<http://www.hakko.co.jp/qa/qakit/html/s01050.htm>

[4] : Method of {pseudo parabola+green house≡PPGH}. Opening area $S_S=1.75m^2$.
 $\{Q_S=956W/m^2 \times 0.25m^2 \times 7=1673W ; S_L=1.5m^2 ; @=0.5\}$. $\rightarrow T_M=[Q_S/S_L@ \sigma]^{1/4}=170^\circ C$
 $\{S_L, @\}$ are green house material of vinyl or glass (IR heat shutter). Heating target (HT=●) must be blackbody.



<<(2)top view>>



(3)The feature of PPGH:

PPGH is to take both merits of parabola antenna and green house box with easy fabrication by flat reflector panels.

$$P_H = Q_S - Q_L = S_S P_S (956W/m^2) - S_L @ \sigma T^4 = E_H / \langle t_H \rangle.$$

$$Q_S = S_S P_S (956W/m^2). \langle \text{solar heat input} \rangle.$$

$$Q_L = S_L @ \sigma T^4. \langle \text{dissipated heat loss} \rangle.$$

$$t_H = E_H / \langle P_H \rangle. \langle \text{heating up time} = \text{total heat amount} / \text{effective heat input} / \text{sec} \rangle.$$

$$T_M = [Q_S / S_L @ \sigma]^{1/4}. \langle \text{max temperature at heat input} = \text{heat loss} \rangle.$$

Parabola anntena (larger S_S , @=1)		Green house (smller S_S , @<1)	
merit	demerit	merit	demerit
higher temperature by beam collection	sensitive for solar direction	de-sensitive?? for solar direction,	lower power input, lower temperature
	smaller volume of heat target (cooking)	larger volume of heat target (cooking)	
	fabrication difficulty	easy fabrication?	green house box fabrication, etc

(4)Maximum green house equibrium temperature in $S_S = S_L$.

solar heat=956W/m ²	= $\sigma T^4 = (@=1.0, \text{max temp})$	= (273 + 87°C) ⁴ .
solar heat=956W/m ²	= $@ \sigma T^4 = (@=0.8, \text{max temp})$	= (273 + 108°C) ⁴ .
solar heat=956W/m ²	= $@ \sigma T^4 = (@=0.7, \text{max temp})$	= (273 + 121°C) ⁴ .
solar heat=956W/m ²	= $@ \sigma T^4 = (@=0.6, \text{max temp})$	= (273 + 136°C) ⁴ .
solar heat=956W/m ²	= $@ \sigma T^4 = (@=0.5, \text{max temp})$	= (273 + 156°C) ⁴ .
solar heat=956W/m ²	= $@ \sigma T^4 = (@=0.4, \text{max temp})$	= (273 + 180°C) ⁴ .

(5)variety of SH in the world.

http://www.google.com/images?hl=en&sugexp=ldymIs&xhr=t&q=solar+cooker&cp=9&rlz=1R2GZAZ_jaJP409&wrapid=tljp1296792789015014&um=1&ie=UTF-8&source=univ&ei=5HxLTd_3IsiHcc6z1NUL&sa=X&oi=image_result_group&ct=title&resnum=2&sqi=2&ved=0CEUQsAQwAQ&biw=955&bih=794

postscript:

Note author had not used and made SH before, so he wish to try it from just now. It's terrible mistake not having the experience. 80% CO2 reduction is possible !.